

**BACHELOR OF TECHNOLOGY IN
MECHANICAL ENGINEERING
(COMPUTER INTEGRATED
MANUFACTURING)**

Term-End Examination

December, 2013

02970

BME-027 : HEAT AND MASS TRANSFER

Time : 3 hours

Maximum Marks : 70

Note : Answer any seven questions . All questions carry equal marks. Use of scientific calculator is permitted.

1. (a) A steam pipe ($\epsilon = 0.85$) of 0.5 m diameter has a surface temperature of 550 K. The pipe is located in a room at 30°C and the convection heat transfer coefficient is 28 W/m²K. Calculate the combined heat transfer coefficient and the rate of heat transfer per unit length of the pipe. 5
- (b) What do you mean by critical radius of insulation ? Derive an expression for critical radius of insulation over a cylinder. 5
2. (a) Define Fick's law of diffusion. Explain how does diffusion take place ? 5
- (b) Distinguish between the surface and volumetric radiation. What is the wavelength range for infra red and visible radiation ? 5

3. (a) Show that the temperature profile for heat conduction through a plane wall with a heat source and constant thermal conductivity is parabolic. 5
- (b) A load of peas at a temperature of 25°C is to be cool down in a room at a constant air temperature of 1°C. How long the peas will require to cool down to 2°C when the surface heat transfer coefficient of the peas is 5.81 W/m²K ? 5
4. (a) One end of a long rod is inserted into a furnace while the other projects into ambient air. Under steady state the temperature of the rod is measured at two points 75 mm apart and found to be 125°C and 88.5°C, respectively, while the ambient temperature is 20°C. If the rod is 25 mm diameter and $h = 23.36 \text{ W/m}^2\text{K}$, find the thermal conductivity of the rod material. 5
- (b) Derive an expression for heat transfer and temperature distribution for a rectangular fin with its tip at adiabatic condition. 5
5. (a) With the help of Buckingham π - theorem show that for forced convection heat transfer 5

$$\text{Nu}_d = C \text{Re}_d^a \text{Pr}^b$$

- (b) A rectangular plate is 120 cm long in the direction of flow and 200 cm wide. The plate is maintained at 80°C when placed in nitrogen that has a velocity of 2.5 m/s and a temperature of 0°C . Determine the average heat transfer coefficient and the total heat transfer from the plate. 5

The properties of Nitrogen at 40°C are $\rho = 10142 \text{ kg/m}^3$, $C_p = 1.04 \text{ kJ/kgK}$; $\nu = 15.63 \times 10^{-6} \text{ m}^2/\text{s}$ and $k = 0.0262 \text{ W/mK}$.

6. (a) Derive an expression for radiation heat transfer for two surface enclosure. What are the assumptions? 5
- (b) Consider a diffuse circular disk of diameter D and area A_j and a plane diffuse surface of area $A_i \ll A_j$. The surfaces are parallel, and A_j is located at a distance L from the centre of A_i . Obtain an expression for the view factor F_{ij} . 5
7. (a) What is evaporation? Draw a sketch of single effect evaporator and explain its working principle. 5
- (b) Explain various application of boiling heat transfer. 5

8. (a) Determine the overall heat transfer coefficient U_o based on the outer surface of a steel pipe with an ID of $D_i = 2.5$ cm and an OD of $D_o = 3.34$ cm [$k = 54$ W/m°C] for the following flow and fouling conditions : 5
- $h_i = 1800$ W/(m² °C) ; $h_o = 1250$ W/m² °C ;
 $F_i = F_o = 0.00018$ m² °C/W

- (b) Consider a cross flow heat exchanger with hot and cold fluids entering at uniform temperatures. Illustrate with sketches the exit temperature distribution for the following cases : 5

- (i) Both fluids are unmixed and
- (ii) Cold fluid is unmixed, hot fluid is mixed.

9. (a) Show that for a mass transfer in a boundary layer over a flat plate is given by : 5

$$Sh = 0.664 Re_L^{1/2} S_C^{1/3}$$

- (b) Explain the phenomenon of equimolar counter diffusion. Derive an expression for equimolar counter diffusion between two gases or liquids. 5

10. (a) A tube is coated on the inside naphthalene and has an inside diameter of 20 mm and a length of 1.10 m. Air at 318 K and an average pressure of 101.3 kPa flows through this pipe at a velocity of 0.8 m/s. Assuming that the absolute pressure remains essentially constant, calculate the concentration of naphthalene in the exit air. Use the physical properties given below :

$$D_{AB} = 6.92 \times 10^{-6} \text{ m}^2/\text{s} \quad \text{Vapour pressure}$$
$$p_{Ai} = 74.0 \text{ Pa} \quad \mu_{\text{air}} = 1.932 \times 10^{-5} \text{ Pa}$$
$$\rho_{\text{air}} = 1.114 \text{ kg/m}^3.$$

- (b) Derive the continuity equation for a binary mixture. 5
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